



# Utilization of simulated flue gas for cultivation of *Scenedesmus dimorphus*

Yinli Jiang, Wei Zhang\*, Junfeng Wang, Yu Chen, Shuhua Shen, Tianzhong Liu\*

Key Laboratory of Biofuels, Qingdao Institute of Bioenergy and Bioprocess Technology, Chinese Academy of Sciences, Qingdao 266101, China

## HIGHLIGHTS

- ▶ *Scenedesmus dimorphus* showed excellent tolerance to high CO<sub>2</sub> (2–20%) and NO concentrations (150–500 ppm).
- ▶ The maximum SO<sub>2</sub> concentration *S. dimorphus* could tolerate was 100 ppm.
- ▶ The extremely low pH as well as the accumulation of bisulfite caused by SO<sub>2</sub> inhibited algae growth.
- ▶ By neutralization with CaCO<sub>3</sub>, *S. dimorphus* could grow well on flue gas.
- ▶ The toxicity of flue gas could be overcome by intermittent sparging and CO<sub>2</sub> utilization efficiency was enhanced.

## ARTICLE INFO

### Article history:

Received 27 April 2012

Received in revised form 3 September 2012

Accepted 8 October 2012

Available online 2 November 2012

### Keywords:

Flue gas

CaCO<sub>3</sub> addition

Intermittent sparging

*Scenedesmus dimorphus*

## ABSTRACT

Effects of flue gas components on growth of *Scenedesmus dimorphus* were investigated and two methods were carried out to eliminate the inhibitory effects of flue gas on microalgae. *S. dimorphus* could tolerate CO<sub>2</sub> concentrations of 10–20% and NO concentrations of 100–500 ppm, while the maximum SO<sub>2</sub> concentration tolerated by *S. dimorphus* was 100 ppm. Addition of CaCO<sub>3</sub> during sparging with simulated flue gas (15% CO<sub>2</sub>, 400 ppm SO<sub>2</sub>, 300 ppm NO, balance N<sub>2</sub>) maintained the pH at about 7.0 and the algal cells grew well (3.20 g L<sup>-1</sup>). By intermittent sparging with flue gas controlled by pH feedback, the maximum biomass concentration and highest CO<sub>2</sub> utilization efficiency were 3.63 g L<sup>-1</sup> and 75.61%, respectively. These results indicated that *S. dimorphus* could tolerate high concentrations of CO<sub>2</sub> and NO, and the methods of CaCO<sub>3</sub> addition and intermittent sparging have great potential to overcome the inhibition of flue gas on microalgae.

© 2012 Elsevier Ltd. All rights reserved.

## 1. Introduction

CO<sub>2</sub> fixation by microalgae is seen as an economically feasible and environmentally sustainable way to mitigate CO<sub>2</sub> emissions and to generate biomass for the productions of biofuels and other chemicals. At least 1.83 tons of CO<sub>2</sub> are needed for obtaining 1 ton of algal biomass (Ho et al., 2010a). Consequently, coupling the cultivation of microalgae with bio-fixation of the CO<sub>2</sub> in flue gas from combustion sources has the potential not only to reduce the cost of microalgae production on an industrial scale but also to offset carbon emissions (de Moraes and Costa, 2007a; Hughes and Benemann, 1997). Typical flue gas emitted from combustion sources contains 10–15% CO<sub>2</sub>, and 100–300 ppm NO<sub>x</sub> and SO<sub>x</sub> (Lee et al., 2002). Some species of microalgae showed little growth inhibition at the typical CO<sub>2</sub> percentages in flue gas (Hanagata et al., 1992; Ho et al., 2010b; Tang et al., 2010), but some other studies showed that growth of

microalgae was inhibited at CO<sub>2</sub> concentrations above 5% (Chiu et al., 2008; de Moraes and Costa, 2007a,b). In contrast, the SO<sub>x</sub> and NO<sub>x</sub> in flue gas, especially from coal-fired power plants, impose more serious inhibition on microalgae (Lee et al., 2002; Negoro et al., 1991). When sparged with a gas mixture containing 300 ppm NO, the growth of *Chlorella* KR-1 was suppressed (Lee et al., 2002), and *Nannochloris* sp. (NANNO02) showed some growth only after a considerable lag time (Negoro et al., 1991). Sulfur oxides, particularly SO<sub>2</sub>, cause a dramatic decline in pH of the culture medium (Lee et al., 2002; Meada et al., 1995). When the SO<sub>2</sub> concentration reaches 400 ppm, the medium pH decreases to below 4 within 24 h, significantly reducing the growth rate of microalgae (Matsumoto et al., 1997). Growth of *Nannochloris* sp. (NANNO02) was strictly inhibited within 20 h at SO<sub>2</sub> concentration of 300 ppm (Negoro et al., 1991).

Several attempts have been made to overcome the toxic effects, more specifically, the acidification of the medium when using flue gas for microalgae cultivation. Some researchers tried to screen NO<sub>x</sub>- and SO<sub>x</sub>-tolerant microalgae or acidophilic algae, but such algae grew consistently only at concentrations of 50 ppm SO<sub>2</sub> or below (Hauck et al., 1996; Kurano et al., 1995). Some researchers

\* Corresponding authors. Tel./fax: +86 532 80662735.

E-mail addresses: [zhangwei@qibebt.ac.cn](mailto:zhangwei@qibebt.ac.cn) (W. Zhang), [liutz@qibebt.ac.cn](mailto:liutz@qibebt.ac.cn) (T. Liu).

have reported that controlling the pH of medium by adding NaOH solution was an effective method to overcome the acid inhibition of flue gas (Lee et al., 2000; Westerhoff et al., 2010); however, neutralization with NaOH not only results in undesirably high ionic strengths which may inhibit growth of microalgae but also makes the cultivation process more complicated and costly.

In the present study, a series of experiments were conducted to investigate the effects of CO<sub>2</sub>, NO, SO<sub>2</sub> on growth of *Scenedesmus dimorphus*, and neutralization by CaCO<sub>3</sub> addition and intermittent sparging of flue gas by pH feedback control were tested to overcome the inhibition of flue gas on microalgal growth.

## 2. Methods

### 2.1. Microalgae cultures

*S. dimorphus* (Chlorophyta, Chlorophyceae), a highly CO<sub>2</sub>-tolerant and fast-growing microalgae, was selected from stock cultures kept in our laboratory. Modified BG-11 medium (Stanier et al., 1971) was used for cultivation of the strain. The medium contained (mg L<sup>-1</sup>): NaNO<sub>3</sub>, 1500; MgSO<sub>4</sub>·7H<sub>2</sub>O, 75; CaCl<sub>2</sub>·2H<sub>2</sub>O, 36; citric acid, 6.0; Na<sub>2</sub>EDTA, 1.0; Ferric ammonium citrate, 6.0; Na<sub>2</sub>CO<sub>3</sub>, 20.0; KH<sub>2</sub>PO<sub>4</sub>·H<sub>2</sub>O, 40.0; ZnSO<sub>4</sub>·7H<sub>2</sub>O, 0.222; CuSO<sub>4</sub>·7H<sub>2</sub>O, 0.079; MnCl<sub>2</sub>·4H<sub>2</sub>O, 1.81; NaMoO<sub>4</sub>·2H<sub>2</sub>O, 0.39; Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, 0.0494; H<sub>3</sub>BO<sub>3</sub>, 2.86.

### 2.2. Experimental system with photobioreactors

The photobioreactors (PBRs) were glass columns (30 mm or 50 mm in diameter; 58 cm in length), which were sparged continuously and kept at 25 ± 1 °C during cultivations. Different column sizes were used over the course of the two-year study for logistical reasons. The columns were illuminated by fluorescent lamps with an intensity of about 100 μmol m<sup>-2</sup> s<sup>-1</sup>, as measured by a Basic Quantum meter (Li-250A light meter, USA). The pH of culture medium was determined by a pH meter (Sartorius PB-10, Germany). For intermittent sparging of flue gas under pH feedback control, the pH meter (405-DAPS-SC-k8s/325, Switzerland) was immersed into the medium and connected to a pH controller (Apure RP-100, China). Flow meters (LZB, China) were utilized to control the flow rates of CO<sub>2</sub>, house air (0.038% CO<sub>2</sub>) and other gases.

In the experiment of intermittent sparging of flue gas, compressed air was continuously supplied to make the culture solution mixed at the aeration rate of 0.25 vvm. The pH value of culture solution was set in a certain range, and regulated by switch on-off mode of flue gas using a pH controller. When the pH reached the minimum point, the aeration of flue gas was switched off automatically, and when the pH reached the maximum point because of the photosynthesis and metabolism of microalgae, the flue gas was automatically sparged again.

### 2.3. Gas mixtures

In the CO<sub>2</sub> experiments, pure CO<sub>2</sub> and house air were mixed to prepare CO<sub>2</sub> concentrations of 0.038%, 2%, 10% and 20%. Since the main constituents of SO<sub>x</sub> and NO<sub>x</sub> are SO<sub>2</sub> and NO, respectively, gas mixtures of 2% CO<sub>2</sub> and different NO concentrations (150, 300, 500 ppm, respectively) were used to evaluate the effect of NO on *S. dimorphus*, while the similar gas mixtures with 2% CO<sub>2</sub> and different SO<sub>2</sub> concentrations (100, 150, 200 ppm, respectively) were used in the SO<sub>2</sub> experiments. Simulated flue gas, with the composition of 15% (v/v) CO<sub>2</sub>, 400 ppm SO<sub>2</sub>, 300 ppm NO and balance N<sub>2</sub>, was adopted in the experiments of CaCO<sub>3</sub> addition and intermittent sparging of flue gas. All the aeration rates were fixed at 0.25 vvm (volume gas/volume liquid/min).

### 2.4. Assay

Optical density of microalgae biomass was measured with a UV/Visible spectrophotometer (UNICO7200, USA) at 730 nm (OD<sub>730</sub>). When necessary, the sample was diluted to give an absorbance in the range of 0.1–1.0. The relationship between optical density and biomass concentration of *S. dimorphus* could be obtained as following:

$$Y = 0.4209X - 0.1189 (R^2 = 0.9987) \quad (1)$$

where Y refers to the biomass concentration (g L<sup>-1</sup>) and X refers to the optical density (OD<sub>730</sub>).

The concentration of total nitrogen concentration in the medium was determined by the method of alkaline potassium persulfate digestion method (Yang et al., 2005).

### 2.5. Determination of CO<sub>2</sub> utilization efficiency

The initial biomass concentration of inoculum and maximum biomass concentration achieved in the PBRs were designated as X<sub>0</sub> and X<sub>max</sub> (g L<sup>-1</sup>), respectively. The biomass concentration ΔX (g L<sup>-1</sup>) over cultivation time of Δt was calculated as ΔX = X<sub>max</sub> - X<sub>0</sub>. The overall biomass productivity P<sub>overall</sub> (g L<sup>-1</sup> d<sup>-1</sup>) was calculated using Eq. (2):

$$P_{\text{overall}} = \frac{\Delta X}{\Delta t} \quad (2)$$

Thus the CO<sub>2</sub> fixation rate F<sub>c</sub> (g CO<sub>2</sub> L<sup>-1</sup> d<sup>-1</sup>) was calculated according to Eq. (3):

$$F_c = \frac{P_{\text{overall}} \times 50\%}{12} \times 44 \quad (3)$$

where 50% is designated as carbon content of microalgae dry biomass; 12 (g/mol) and 44 (g/mol) present the molecular weights of carbon and CO<sub>2</sub>, respectively.

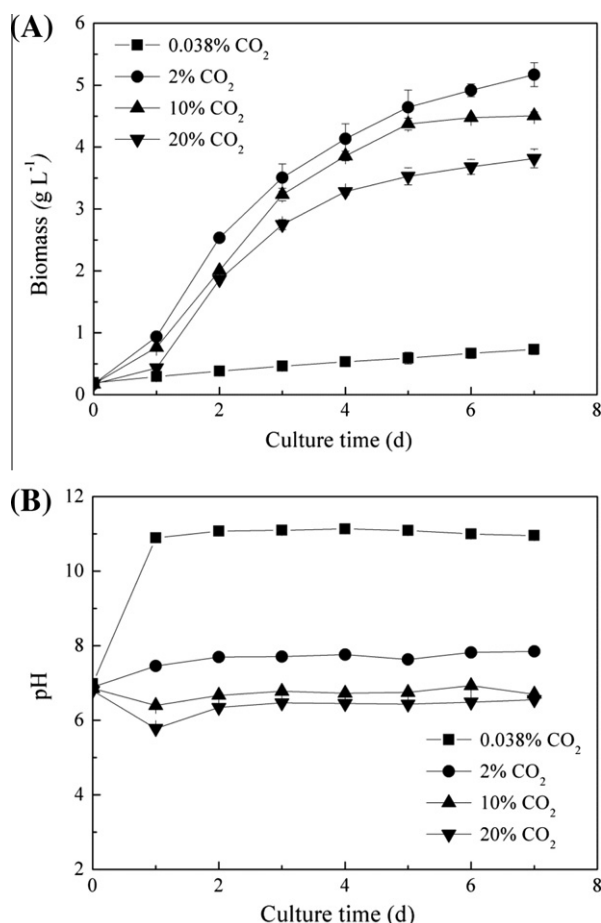
The total CO<sub>2</sub> amount injected into the culture medium included all the CO<sub>2</sub> introduced into the bubbling column, including CO<sub>2</sub> in mixed gas (pure CO<sub>2</sub>-air or flue gas) and air for stirring. For each pH feedback control experiment with flue gas, the aeration time and total time per cycle each day were measured, and the total CO<sub>2</sub> amount from the flue gas could be calculated (M<sub>c1</sub>, g); the compressed house air (0.038% CO<sub>2</sub>) was continuously injected (0.25 vvm) to keep the culture medium mixed, so the total CO<sub>2</sub> from the air could be obtained (M<sub>c2</sub>, g). The CO<sub>2</sub> utilization efficiency E<sub>c</sub> (%) was derived from Eq. (4):

$$E_c = \frac{F_c}{M_{c1} + M_{c2}} \times 100\% \quad (4)$$

## 3. Results and discussion

### 3.1. Effect of CO<sub>2</sub> concentration on microalgae growth

Industrial exhaust gases such as flue gases contain 10–20% CO<sub>2</sub>, providing a CO<sub>2</sub>-rich source for microalgae cultivation and a potentially more efficient route for CO<sub>2</sub> bio-fixation (Wang et al., 2008). To demonstrate the tolerance of *S. dimorphus* for high CO<sub>2</sub> concentration, growth experiments were carried out under CO<sub>2</sub> concentrations of 0.038%, 2%, 10%, 20% CO<sub>2</sub> (v/v). The PBR was a 300-ml bubble column (30 mm in diameter) with a 200-ml working volume. The initial inoculum concentration was about 0.2 g L<sup>-1</sup> and the pH was unregulated (7.0 ± 0.2). As shown in Fig. 1, growth of *S. dimorphus* sparged with 0.038% CO<sub>2</sub> was slow, while the cells grew well with CO<sub>2</sub> concentrations ranging from 2% to 20%. The pH changes of culture media with 2% to 20% CO<sub>2</sub> tended to be stable at around 6–8 after 1 day of cultivation. In the culture aerated



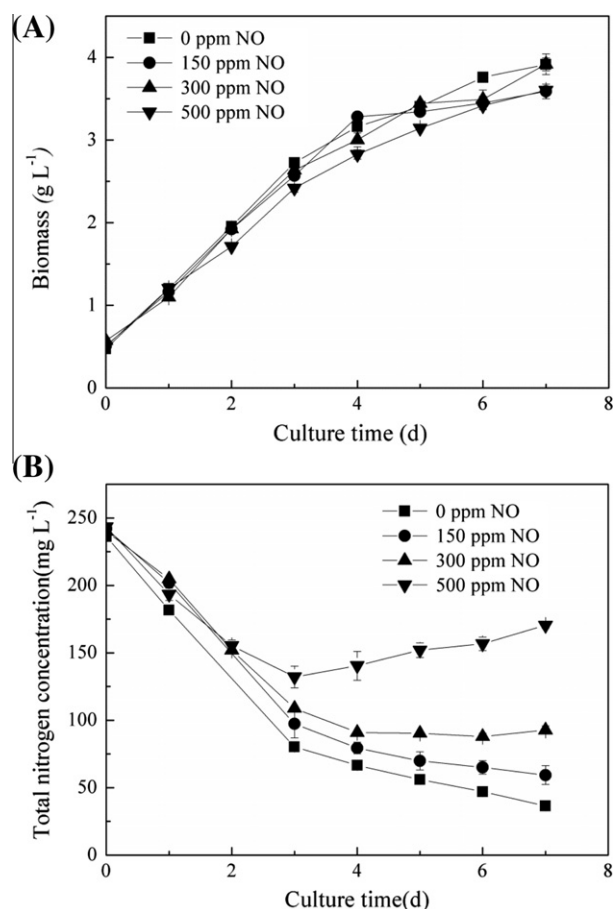
**Fig. 1.** Growth (A) and pH (B) of cultures of *S. dimorphus* sparged with 0.038%, 2%, 10%, or 20% CO<sub>2</sub> (column diameter = 30 mm). Values are means  $\pm$  SD of three repeated experiments.

with house air, the pH value increased from 7 to about 11 within one day. It appears that the concentration of 0.038% CO<sub>2</sub> in house air was too low to neutralize alkaline substances produced by the micro-algae and carbon limitation may also have occurred.

Chiu et al. reported that *Chlorella* sp. (Chiu et al., 2008) and *Nannochloropsis oculata* (Chiu et al., 2009) showed optimal growth potential with 2% CO<sub>2</sub>, while growths of both algal strains were completely inhibited at 5–15% CO<sub>2</sub>. In the present study, *S. dimorphus* grew well with 2–20% CO<sub>2</sub>, and the maximum biomass concentration of 5.17 g L<sup>-1</sup> was observed with 2% CO<sub>2</sub>. *S. dimorphus* exhibited a longer lag phase when sparged with 10 and 20% CO<sub>2</sub>, and the biomass concentrations after 7 days of cultivation were 4.51 and 3.82 g L<sup>-1</sup>, respectively. Tang et al. (2010) reported that *Scenedesmus obliquus* SJTU-3 and *Chlorella pyrenoidosa* SJTU-2 grew well at CO<sub>2</sub> concentrations ranging from 5% to 30%, and the biomass concentrations of *S. obliquus* SJTU-3 and *C. pyrenoidosa* SJTU-2 at 20% CO<sub>2</sub> after 14 days of cultivation were 1.65 g L<sup>-1</sup> and 1.22 g L<sup>-1</sup>, respectively, which were much lower than that of *S. dimorphus* in our study. For most flue gas sources, the CO<sub>2</sub> concentrations were generally below 20% (Lee et al., 2002; Westerhoff et al., 2010), under which *S. dimorphus* screened in our study showed excellent growth potential.

### 3.2. Effects of NO and SO<sub>2</sub> concentration on microalgae growth

Effects of different NO concentrations on *S. dimorphus* were showed in Fig. 2A. *S. dimorphus* grew well at NO concentrations of 150–500 ppm, similarly as with control cultures with 2% CO<sub>2</sub>

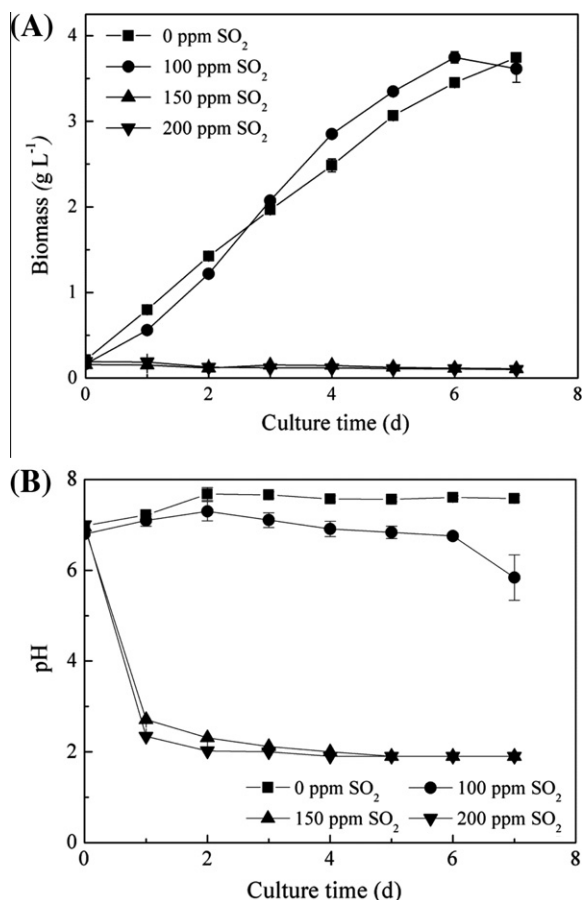


**Fig. 2.** Growth of *S. dimorphus* (A) and total nitrogen concentration (B) in medium supplied with 0, 100, 150, 300, 500 ppm NO (column diameter = 50 mm). Values are means  $\pm$  SD of three repeated experiments.

alone. Changes of total nitrogen concentrations in the medium during microalgae growth were showed in Fig. 2B. The results showed that at higher NO concentration, the consumption rate of total nitrogen concentration was slower, indicating that NO might be used as nitrogen source for algal cells (Kumar et al., 2010).

As shown in Fig. 3A, *S. dimorphus* only grew well when SO<sub>2</sub> concentrations were lower than 100 ppm. When the SO<sub>2</sub> concentration exceeded 100 ppm, the pH of culture medium dropped to 3 within one day (Fig. 3B). Experiments were then conducted with addition of sodium sulfite and sodium bisulfite, respectively, instead of gaseous SO<sub>2</sub>. As shown in Fig. 4, *S. dimorphus* could grow well at sulfite concentrations of 0–60 mmol/L, while the maximum bisulfite concentration *S. dimorphus* could tolerate was only 1.0 mmol/L. Similar results were reported by Yang et al. (2004), bisulfite was toxic to *Botryococcus braunii* when the concentration was above 1.0 mmol/L. Wodzinski et al. (1978) reported that the toxicity of bisulfite-sulfite increased as the pH decreased, and as the pH decreased from 7.7 to 6.0, the bisulfite-sulfite ratio changed from 0.16:1 to 8.1:1. At the extremely low pH caused by large amount of dissolved SO<sub>2</sub> gas, there was a higher proportion of bisulfite than that of sulfite in the solution. Therefore, limiting the accumulation of bisulfite in solution is essential to prevent growth inhibition on microalgae.

Negoro et al. (1991) reported that growth of *Nannochloris* sp. (NANNO<sub>2</sub>) and *Nannochloropsis* sp. (NANNP2) was not influenced by SO<sub>2</sub> at a concentration of 50 ppm, while growth ceased after 20 h cultivation when the SO<sub>2</sub> concentration was increased to 400 ppm. Lee et al. (2002) reported that growth of *Chlorella* KR-1



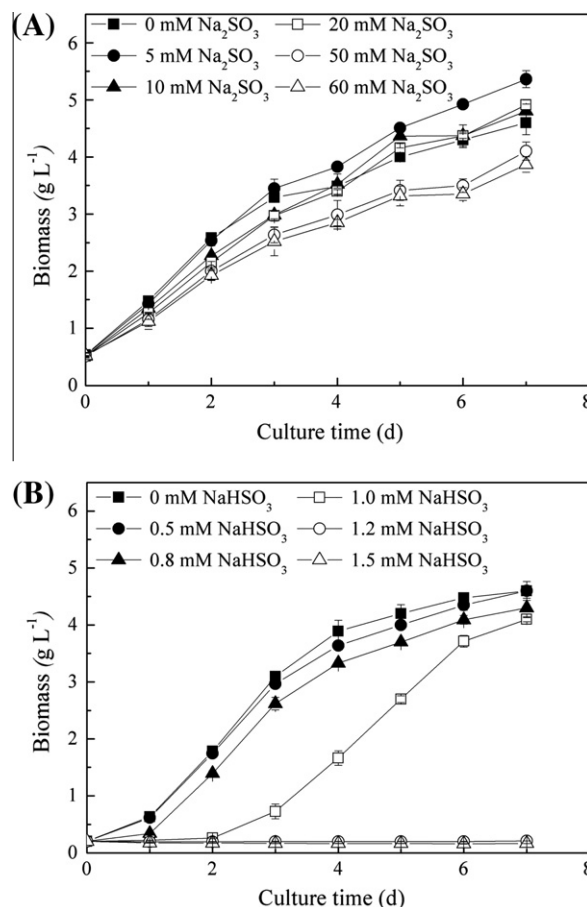
**Fig. 3.** Growth (A) and pH (B) of cultures of *S. dimorphus* supplied with 0, 100, 150, 200 ppm SO<sub>2</sub> (column diameter = 50 mm). Values are means  $\pm$  SD of three repeated experiments.

was totally inhibited by 150 ppm SO<sub>2</sub>. Westerhoff et al. (2010) reported that *Scenedesmus*, *Chlorella* or a mixture of the two cultures died almost immediately upon gaseous addition of 313 ppm SO<sub>2</sub> in 20% CO<sub>2</sub>. Nitrous oxides were also present in the flue gas. When the NO concentration was 300 ppm, NANNP2 did not grow and NANN02 grew only after a prolonged lag period (Negoro et al., 1991), and growth of *Chlorella* KR-1 was also completely suppressed (Lee et al., 2002). In the present study, the maximum NO and SO<sub>2</sub> concentrations *S. dimorphus* could tolerate were 500 ppm and 100 ppm, respectively, which are much higher than those reported in previous studies (Lee et al., 2002; Negoro et al., 1991; Westerhoff et al., 2010). However, considering that typical industrial flue gases usually contain 100–300 ppm SO<sub>x</sub> and NO<sub>x</sub>, it is necessary to develop strategies to overcome the adverse effects of flue gas on microalgae growth.

### 3.3. Methods to overcome the toxic effect of flue gas on *S. dimorphus*

#### 3.3.1. Neutralization of the medium with CaCO<sub>3</sub>

Though complete removal of SO<sub>x</sub> and NO<sub>x</sub> in flue gas by washing with an alkaline solution prior to injecting into the culture medium would be feasible, the consumption and recycling of absorbing agents would result in high costs. Inspired by the process of wet limestone flue gas desulfurization, adding CaCO<sub>3</sub> to culture medium was tested as a means of neutralizing the acidification caused by SO<sub>2</sub> in flue gas. For each column with 700 ml culture broth, 3.15 g CaCO<sub>3</sub> was added. The amount of CaCO<sub>3</sub> was determined by the stoichiometric ratio of 1:1 with



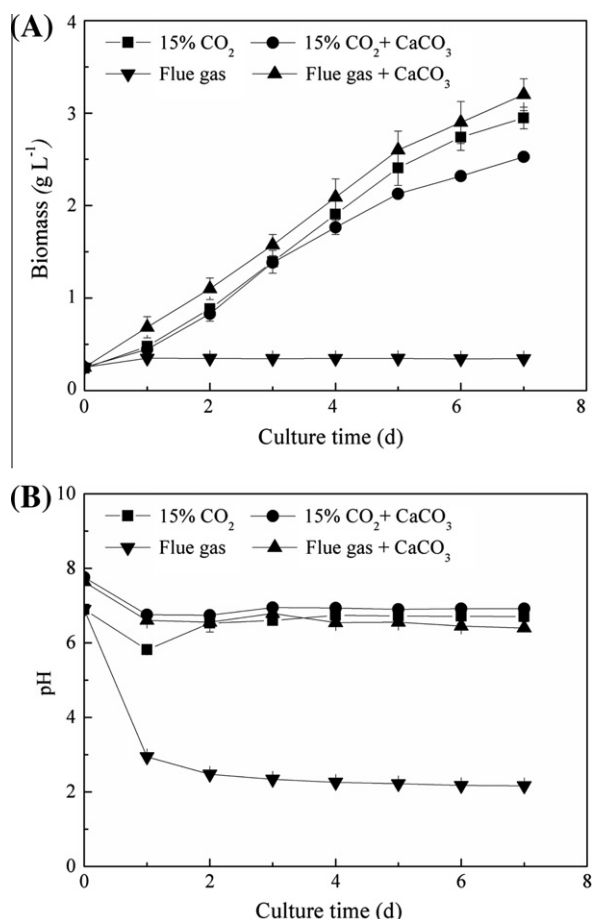
**Fig. 4.** Effects of Na<sub>2</sub>SO<sub>3</sub> (A) and NaHSO<sub>3</sub> (B) on growth of *S. dimorphus* supplied with 2% CO<sub>2</sub> (column diameter = 30 mm). Values are means  $\pm$  SD of three repeated experiments.

the entire SO<sub>2</sub> amount in flue gas for 7 d cultivation. Upon addition of CaCO<sub>3</sub>, the pH of media sparged with simulated flue gas stabilized at above 6 and the cells grew very well (Fig. 5). Interestingly, with CaCO<sub>3</sub> addition, the biomass concentration of *S. dimorphus* with flue gas was 3.20 g L<sup>-1</sup>, 27% higher than that of the control culture with pure CO<sub>2</sub>-air gas sparging. Meada et al. (1995) found that the pH could be maintained neutral with CaCO<sub>3</sub> addition when cultivating *Chlorella* sp. T-1 with flue gas containing 50 or 80 ppm SO<sub>2</sub>; however, the aeration time was only 70 h. Limestone powder, whose main component is CaCO<sub>3</sub> can be adopted instead of pure CaCO<sub>3</sub> because of its rich source and lower price. Putt et al. (2011) observed a low CO<sub>2</sub> utilization efficiency when CO<sub>2</sub>-enriched air was continuously supplied into algae ponds; however, with measures to increase the CO<sub>2</sub> utilization efficiency, such as decreasing the aeration rate and CO<sub>2</sub> concentration (Ryu et al., 2008), intermittent aeration (Chiu et al., 2011), the required stoichiometric amount of CaCO<sub>3</sub> to neutralize the SO<sub>2</sub> would be greatly reduced. The produced CaSO<sub>4</sub> precipitate could be easily separated by centrifugation, with little influence on the growth of algal cells and the quality of microalgae product.

#### 3.3.2. Intermittent sparging of flue gas by pH feedback

Since *Scenedesmus* sp. prefers a slightly alkaline medium (Hodaifa et al., 2009), three pH ranges were adopted in this study: pH 8.0–8.5, pH 8.5–9.0 and pH 9.0–9.5. Growth of *S. dimorphus* at different pH regimes was compared with control cultures continuously sparged with simulated flue gas or 15% CO<sub>2</sub>. Fig. 6A shows the pH variations of *S. dimorphus* cultures supplied with different





**Fig. 5.** Biomass concentration (A) and pH (B) of cultures of *S. dimorphus* exposed to simulated flue gas (15% CO<sub>2</sub>, 400 ppm SO<sub>2</sub>, 300 ppm NO, balance N<sub>2</sub>) with or without CaCO<sub>3</sub> addition (column diameter = 50 mm). Values are means  $\pm$  SD of three repeated experiments.

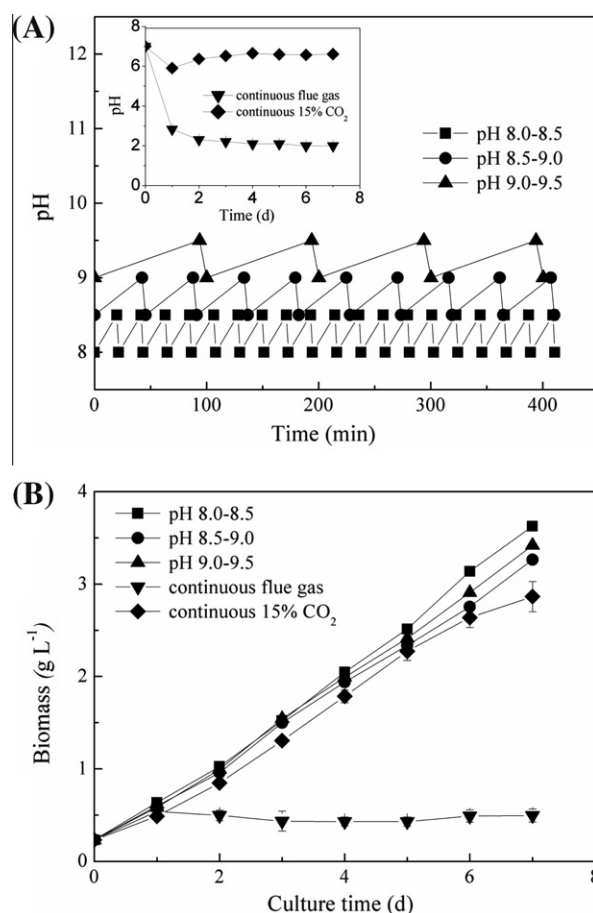
**Table 1**

Comparison of growth and CO<sub>2</sub> utilization of *S. dimorphus* supplied with different gas mixtures (flue gas composition: 15% CO<sub>2</sub>, 400 ppm SO<sub>2</sub>, 300 ppm NO, balance N<sub>2</sub>; column diameter = 50 mm). Values are means  $\pm$  SD of three repeated experiments.

Aeration modes		$X_{max}$ (g L <sup>-1</sup> )	$P_{overall}$ (g L <sup>-1</sup> d <sup>-1</sup> )	$F_C$ (g CO <sub>2</sub> L <sup>-1</sup> d <sup>-1</sup> )	$E_C$ (%)
Intermittent sparging of flue gas by pH feedback	pH 8.0–8.5	3.63	0.485	0.889	75.61*
	pH 8.5–9.0	3.36	0.448	0.821	65.29*
	pH 9.0–9.5	3.42	0.455	0.835	67.71*
Continuous aeration	15% CO <sub>2</sub>	2.77	0.362	0.664	1.60
	Flue gas	0.49	0.037	0.068	0.17

\* The total carbon supplied was calculated from the aerated CO<sub>2</sub> amount from both flue gas and compressed air for stirring.

gas mixtures. The pH value with continuous 15% CO<sub>2</sub> stabilized at around 6.5, while the pH with continuous flue gas dropped to around 3 after 1 d of cultivation. For the three pH-controlled experiments, the fastest sparging frequency was observed when the feedback pH was set at pH 8.0–8.5, and the slowest sparging frequency was at pH 9.0–9.5. In the pH range of 8.0–9.5, the main carbon form in solution is HCO<sub>3</sub><sup>-</sup>. At a higher pH, the culture has a higher buffering capacity which could explain the low sparging frequency at pH range 9.0–9.5. All the pH feedback-controlled cultures of pH controlling achieved higher growth rates than those with continuous 15% CO<sub>2</sub> sparging (Fig. 6B). As shown in Table 1, the maximum biomass concentration, CO<sub>2</sub> fixation rate and CO<sub>2</sub> utilization efficiency of 3.63 g L<sup>-1</sup>, 0.889 g d<sup>-1</sup> and 75.61%, respec-



**Fig. 6.** (A) pH of culture medium under continuous and intermittent sparging with simulated flue gas on day 7. (B) Growth of *S. dimorphus* under different culture conditions (flue gas composition: 15% CO<sub>2</sub>, 400 ppm SO<sub>2</sub>, 300 ppm NO, balance N<sub>2</sub>; column diameter = 50 mm). Values are means  $\pm$  SD of three repeated experiments.

tively, were obtained at pH 8.0–8.5, while the corresponding values were only 2.77 g L<sup>-1</sup>, 0.664 g d<sup>-1</sup> and 1.6% with 15% CO<sub>2</sub> sparging. Bao et al. (2012) reported that, in the cultivation of *Spirulina platensis* with CO<sub>2</sub> aeration by pH feedback, the pH was maintained at the range of 9.7–9.9, and the maximum biomass concentration and average CO<sub>2</sub> utilization efficiency were 0.84 g L<sup>-1</sup> and 79.18%, respectively. Currently, the major drawback of using CO<sub>2</sub> for large-scale microalgae cultivation is the low CO<sub>2</sub> utilization efficiency. It has been reported that 80–90% of the CO<sub>2</sub> would eventually be lost to the atmosphere (Putt et al., 2011), which makes microalgae production costly. In the present study, the strategy of intermittent sparging of flue gas by pH feedback not only relieved the acidic inhibition of flue gas on microalgae but also enhanced the CO<sub>2</sub> utilization efficiency.

#### 4. Conclusions

In this work, *S. dimorphus* showed excellent tolerance to flue gas containing high concentrations of CO<sub>2</sub> (2–20%) and NO (150–500 ppm), and the maximum SO<sub>2</sub> concentration *S. dimorphus* could tolerant was 100 ppm. The extremely low pH as well as the accumulation of bisulfite caused by SO<sub>2</sub> inhibited algae growth. Upon addition of CaCO<sub>3</sub> and intermittent sparging of flue gas controlled by pH feedback, the inhibition of flue gas on *S. dimorphus* could be well overcome and algal cells grew well (>3 g L<sup>-1</sup>), indicating that these two methods have great potential when using flue gas for microalgae cultivation.

## Acknowledgements

This work was supported by the Key Technologies R&D Program from Ministry of Science and Technology of China (2011BAD14B01), Solar Energy Initiative Plan (KG CX-eW-309), and International Innovation Partnership Program from Chinese Academy of Sciences.

## References

- Bao, Y., Liu, M., Wu, X., Cong, W., Ning, Z., 2012. *In situ* carbon supplementation in large-scale cultivation of *Spirulina platensis* in open raceway pond. *Biotechnol. Bioprocess Eng.* 17, 93–99.
- Chiu, S.-Y., Kao, C.-Y., Chen, C.-H., Kuan, T.-C., Ong, S.-C., Lin, C.-S., 2008. Reduction of CO<sub>2</sub> by a high-density culture of *Chlorella* sp. in a semicontinuous photobioreactor. *Bioresour. Technol.* 99 (9), 3389–3396.
- Chiu, S.-Y., Kao, C.-Y., Tsai, M.-T., Ong, S.-C., Chen, C.-H., Lin, C.-S., 2009. Lipid accumulation and CO<sub>2</sub> utilization of *Nannochloropsis oculata* in response to CO<sub>2</sub> aeration. *Bioresour. Technol.* 100 (2), 833–838.
- Chiu, S.-Y., Yao, C.-Y., Huang, T.-T., Lin, C.-J., Ong, S.-C., Chen, C.-D., Chang, J.-S., Lin, C.-S., 2011. Microalgal biomass production and on-site bioremediation of carbon dioxide, nitrogen oxide and sulfur dioxide from flue gas using *Chlorella* sp. cultures. *Bioresour. Technol.* 102, 9135–9142.
- de Morais, M.G., Costa, J.A.V., 2007a. Biofixation of carbon dioxide by *Spirulina* sp. and *Scenedesmus obliquus* cultivated in a three-stage serial tubular photobioreactor. *J. Biotechnol.* 129 (3), 439–445.
- de Morais, M.G., Costa, J.A.V., 2007b. Isolation and selection of microalgae from coal fired thermoelectric power plant for biofixation of carbon dioxide. *Energy Convers. Manage.* 48 (7), 2169–2173.
- Hanagata, N., Takeuchi, T., Fukujii, Y., Barnes, D.J., Karube, I., 1992. Tolerance of microalgae to high CO<sub>2</sub> and high temperature. *Phytochemistry* 31 (10), 3345–3348.
- Hauck, J.T., Scierka, S.J., Perry, M.B., 1996. Effects of simulated flue gas on growth of microalgae. 212th national meeting of the American Chemical Society (ACS), Orlando, FL (United States) 41 (4), 1391–1396.
- Ho, S.-H., Chen, C.-Y., Lee, D.-J., Chang, J.-S., 2010a. Perspectives on microalgal CO<sub>2</sub>-emission mitigation systems - a review. *Biotechnol. Adv.* 29 (2), 189–198.
- Ho, S.-H., Chen, W.-M., Chang, J.-S., 2010b. *Scenedesmus obliquus* CNW-N as a potential candidate for CO<sub>2</sub> mitigation and biodiesel production. *Bioresour. Technol.* 101 (22), 8725–8730.
- Hodaifa, G., Martínez, M.E., Sánchez, S., 2009. Influence of pH on the culture of *Scenedesmus obliquus* in olive-mill wastewater. *Biotechnol. Bioprocess Eng.* 14, 854–860.
- Hughes, E., Benemann, J.R., 1997. Biological fossil CO<sub>2</sub> mitigation. *Energy Convers. Manage.* 38, S467–S473.
- Kumar, A., Ergas, S., Yuan, X., Sahu, A., Zhang, Q., Dewulf, J., Malcata, F.X., van Langenhove, H., 2010. Enhanced CO<sub>2</sub> fixation and biofuel production via microalgae: recent developments and future directions. *Trends Biotechnol.* 28 (7), 371–380.
- Kurano, N., Ikemoto, H., Miyashita, H., Hasegawa, T., Hata, H., Miyachi, S., 1995. Fixation and utilization of carbon dioxide by microalgal photosynthesis. *Energy Convers. Manage.* 36 (6–9), 689–692.
- Lee, J.-N., Lee, J.-S., Shin, C.-S., Park, S.-C., Kim, S.-W., 2000. Methods to enhance tolerances of *Chlorella* KR-1 to toxic compounds in flue gas. *Appl. Biochem. Biotechnol.* 84–86 (1), 329–342.
- Lee, J.-S., Kim, D.-K., Lee, J.-P., Park, S.-C., 2002. Effects of SO<sub>2</sub> and NO on growth of *Chlorella* sp. KR-1. *Bioresour. Technol.* 82, 1–4.
- Matsumoto, H., Hamasaki, A., Sioji, N., Ikuta, Y., 1997. Influence of CO<sub>2</sub>, SO<sub>2</sub> and NO in flue gas on microalgae productivity. *J. Chem. Eng. Jpn.* 30 (4), 620–624.
- Mead, K., Owada, M., Kimura, N., Omata, K., Karube, I., 1995. CO<sub>2</sub> fixation from the flue gas on coal-fired thermal power plant by microalgae. *Energy Convers. Manage.* 36, 717–720.
- Negoro, N., Shioji, N., Miyamoto, K., 1991. Growth of microalgae in high CO<sub>2</sub> gas and effects of SO<sub>x</sub> and NO<sub>x</sub>. *Appl. Biochem. Biotechnol.* 28, 877–886.
- Putt, R., Singh, M., Chinnasamy, S., Das, K.C., 2011. An efficient system for carbonation of high-rate algae pond water to enhance CO<sub>2</sub> mass transfer. *Bioresour. Technol.* 102 (3), 3240–3245.
- Ryu, H.J., Oh, K.K., Kim, Y.S., 2008. Optimization of the influential factors for the improvement of CO<sub>2</sub> utilization efficiency and CO<sub>2</sub> mass transfer rate. *J. Ind. Eng. Chem.* 15, 471–475.
- Stanier, R.Y., Kunisawa, R., Mandel, M., Cohen-Bazier, G., 1971. Purification and properties of unicellular blue-green algae (order Chroococcales). *Bacteriol. Rev.* 35 (2), 171–205.
- Tang, D., Han, W., Li, P., Miao, X., Zhong, J., 2010. CO<sub>2</sub> biofixation and fatty acid composition of *Scenedesmus obliquus* and *Chlorella pyrenoidosa* in response to different CO<sub>2</sub> levels. *Bioresour. Technol.* 102, 3071–3076.
- Wang, B., Li, Y., Wu, N., Lan, C.Q., 2008. CO<sub>2</sub> bio-mitigation using microalgae. *Appl. Microbiol. Biotechnol.* 79 (5), 707–718.
- Westerhoff, P., Hu, Q., Esparza-Soto, M., Vermaas, W., 2010. Growth parameters of microalgae tolerant to high levels of carbon dioxide in batch and continuous-flow photobioreactors. *Environ. Technol.* 31 (5), 523–532.
- Wodzinski, R.S., Labeda, D.P., Alexander, M., 1978. Effects of low concentrations of bisulfite-sulfite and nitrite on microorganisms. *Appl. Environ. Microbiol.* 35 (4), 718–723.
- Yang, S., Kang, R., Cong, W., 2005. Effect of nitrite and bisulfite on the growth of *Botryococcus braunii*. *Chin. J. Bioprocess Eng.* 3 (1), 49–53.
- Yang, S., Wang, J., Cong, W., Cai, Z., Ouyang, F., 2004. Effects of bisulfite and sulfite on the microalga *Botryococcus braunii*. *Enzyme Microb. Technol.* 35, 46–50.